

# Study of Ceramic and Hybrid Coatings Produced by the Sol-Gel Method for Corrosion Protection

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**Abstract:** Silica based ceramic oxides and hybrid coatings were developed using 3-(trimethoxysilyl) propylmethacrylate (TMSPM), methylmethacrylate (MMA) as the organic phase with different fractions of tetraethoxysilane (TEOS) and aluminium isopropoxide as the inorganic phase using sol-gel process which were deposited onto 316 stainless steel substrate by dip-coating technique, followed by a sintering step. Characterization of the obtained coatings was carried out by scanning electron microscopy to determine the topographical features of the coatings. Furthermore, the coatings were analyzed in this manner after the corrosion tests. Analyses of corrosion resistance for coated and uncoated samples were performed in  $\text{SO}_4^{2-}$  and  $\text{Cl}^-$  solutions. The influence of the sol characteristic and composition, as well as the behaviour of the coatings during the corrosion tests were reported. The results show that coatings prevent corrosion in an acid environment, and the ceramic coating developed best resistance corrosion under those media.

**Keywords:** Thin films, ceramic mix-oxide, hybrid, coatings, sol-gel, dip-coating, corrosion, stainless steel, acid medium, electrochemical tests.

## INTRODUCTION

One of the most interesting applications of the sol-gel method is the deposition of thin oxide layer on glass, ceramic or metal substrates. In the literature, there are many examples showing the versatility and the simplicity of this method to produce coatings for many different purposes [1, 2]. The coatings like hybrid mix-up improve the chemical and physical properties of the metal surfaces relative to corrosion, friction and wear performance without altering the original properties such as strength and toughness of the substrate [3]. During sol-gel thin film formation *via* dipping, inorganic or metal organic sol is deposited on the substrate surface by a complex steady-state process combining gravitational draining, solvent evaporation and continued condensation reactions [4, 5].

The properties of the hybrids are not just the direct addition of the individual contributions from inorganic and organic components. The use of synergistic effects by combining both components can lead to the innovation of multifunctional materials. A wide versatility in the design of the inorganic-organic hybrids provides various applications

of these materials in the fields of optics, electronics, mechanics, biology and others [6]. The inorganic component in the hybrid films has reinforced the organic component enhancing hardness and consequently more abrasion resistant films are achieved compared to the pure PMMA-films [7]. The presence of organic components turns the gel network into a more flexible and less prone to crack film during further heat-treatment. Moreover, the impregnation of open pores by organic materials can reduce the coating porosity producing a better diffusion barrier [8].

It is possible to hybridize ceramics and polymers using a relatively new low-temperature method for ceramic processing. This sol-gel process involves the formation of an inorganic glass from solution and yields a high-purity homogeneous ceramic material [9, 10]. One successful approach to hybridization has been to use the sol-gel process to polymerize metal alkoxides in organic polymer matrices [11-17]. In addition, this process can be used to prepare an inorganic-organic hybrid coating through the *in situ* polycondensation of a metal alkoxide in an inorganic polymer matrix [18, 19].

The coatings of metallic surfaces by sol-gel films have been proposed as a useful way to protect against acid corrosion [20]. The barrier coated *via* sol-gel process consists of the preparation of a solution (sol), from which the

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gel is obtained and applied by several methods to protect the surfaces [21-26]. The deposition of these thin films can offer some advantages in devices, particularly in the case of integrated hybrid systems. Homogeneous thin films could be prepared by dipping process using alkoxides. The metal alkoxide method offers many advantages such as: high purity, low-temperature processing and controllability of the composition [22, 23, 27]. The dipping process is one of the deposition methods involving liquid films [28, 29]. Sol-gel dip-coating has been used to develop corrosion resistance on structural metallic components, like low carbon steels [22, 23] showing good performance in corrosion protection into environments of chemical industry. In industrial applications sulphuric acid is one of top products of the chemical industry like: fertilizer manufacturing, oil refining wastewater processing, and chemical synthesis of many kinds [30]. Additionally, it is a constituent of acid rain which is formed by atmospheric oxidation of sulphur dioxide (from combustion oil process, as an example) in the presence of water, i.e., oxidation of sulphuric acid). In this sense, chlorine acid solution can be present in the processes of chemical intermediate in other chemical production (of hydrochloric acid), hydrochlorination of rubber, production of vinyl and alkyl chlorides, etc. All those industrial acid conditions are the promoters of the structural material corrosion, and are necessary a form of material protection or corrosion inhibition; which can be obtained by the surface modification by sol-gel coatings.

In this work, the results of a systematic corrosion study by electrochemical dynamic-polarization tests of sol-gel coatings of ceramic mix-oxide and hybrid coatings deposited on stainless steel 316 by dip coating technique in acid environments ( $H_2SO_4$  and HCl solutions at 1.0 M and 0.1 M concentrations) are presented. The results were complemented by SEM characterization.

## METHODOLOGY

A simple method to obtain organic-inorganic hybrids is by mixing an organic polymer with a silicon alkoxide such as tetraethoxysilane (TEOS) as the silicate source; followed by sol-gel reaction involving hydrolysis and polycondensation of TEOS [29].

### Materials

Samples of stainless steels 316 were used as substrate in the metal/coating system. Tetraethoxysilane (TEOS, 99% Aldrich) was used as the silica source. 3-(trimethoxysilyl) propylmethacrylate (TMSPM, 98% Aldrich) and methylmethacrylate (MMA, 99% Aldrich), were used as the polymer component. HCl was used as the catalyst is (2,2' Azobisisobutyronitrile) for hydrolysis. The metal alkoxide of aluminium (aluminium isopropoxide, AIP, 98% Aldrich) was used for preparing the ceramic coating. The chemical composition of stainless steel 316 (SS 316) used as coating substrate is: Fe (balance), <0.03% C, 16-18.5% Cr, 10-14% Ni, 2-3% Mo, <2% Mn, <1% Si, <0.045% P, <0.03% S. The substrate was selected due to its corrosion resistance known characteristics, in order to minimize substrate signals and differentiated the coating behaviour. Pieces of 40 x 20 mm<sup>2</sup> from 1.0 mm of thickness foil were cut and surface finished by polished, cleaned and degreased with isopropyl alcohol and air-dried.

## Sol Preparation

**Preparation of  $M_1$  sol:** The silica-sol was prepared by acid-catalysed hydrolysis of tetraethylorthosilicate (TEOS) in ethanol and in the presence of HCl. This sol was reflux under heating for 3 hours. Next, 0.2 g of AIP (aluminium isopropoxide) dissolved in ethanol was added. The resultant mixture was heated to 76°C for 3 hours under reflux. The molar ratio Si:Al was 2:1.

**Preparation of  $C_1$  sol:** First, the copolymerization of MMA and TMSPM is carried out in nitrogen atmosphere and using AIBN (2,2' Azo Bis Iso Butilonitrilo) as an initiator at 70°C during 60 minutes. The obtained liquid is diluted in methanol, and TEOS is slowly added in the appropriate quantity. For the hydrolysis reaction at ambient temperature, acid water is added (0.15 N HCl), using an equivalent of water for alkoxide group. Finally, the previously dissolved AIP is added in hot ethanol (80°C) and it is allowed that the formation reaction is made of the mixed oxide  $SiO_2-Al_2O_3$  to ambient temperature for 3 hours. The molar ratio Si:Al is 2:1.

## Coating Procedure

Steel substrates (10x10x0.1 cm) were polished, cleaned and degreased with isopropyl alcohol and air-dried. The two prepared sol solutions were used to deposit the sol onto the substrates by dip-coating technique. Each substrate was dipped into the sol at an immersion speed of 20 cm/min for 5 minutes, and then withdrawn at the same speed previously mentioned. After deposition, the coated samples were air-dried and heat treated at 600°C for 2 hours by heating rate of 2°C/min, as before reported [31]. Similarly, the hybrid coatings were dried at room temperature and then heat treated at 200°C. The SS 316 alloy used as substrate, is characterized as extra-low-carbon and is stabilized grade stainless steel (with 0.030 wt. % of carbon) [32], and this material is required to be heat treated at 650 to 675°C in order to be sensitized, although, the most commonly used sensitizing treatment is 1 hour at 675°C. However, for this stainless steel alloy, the sensitizing appears after the 50 hours at 650°C [33]. Because of the heat treatment minimum changes were expected in the substrate.

## Corrosion Analysis

The corrosion resistance analyzes of the coated samples which were carried out by the electrochemical polarization technique using a computerized potentiostat (ACM Instruments). The electrochemical cell consisted of a saturated calomel electrode (SCE) used as a reference electrode, a graphite foil used as auxiliary electrode and the work electrode was each coated sample. Work electrode area exposed to the electrolyte was 1.0 cm<sup>2</sup>, for each specimen, the rest of sample surface was insulated with epoxy paint. The potentiodynamic measurements were initiated at -200 mV and ended at 1500 mV from the open circuit potential with a scanning rate of 1 mV/s. The electrolyte solutions were  $H_2SO_4$  and HCl in both 1.0 and 0.1 M concentrations at room temperature. In addition, Scanning electronic microscopy (SEM, JEOL JSM5800 LV) was used to study topographical features and the homogeneity of surface analysis.

## RESULTS AND DISCUSSION

Fig. (1) shows an example of the surface morphology of one coating applied onto the substrate; similar morphologies were obtained by all coatings. In this figure the SEM micrograph of the  $\text{SiO}_2\text{-Al}_2\text{O}_3$  coating (sample  $M_1$ ) obtained by the dip-coating technique followed by the heat treatment (Fig. 1) is shown. SEM micrographs show uniform, homogeneous and crack-free surfaces of sol-gel coatings, which were readily obtained after post-deposition annealing. The morphology of the ceramic coatings showed a completely covered surface, following similar surface topography in accordance with the polished surface texture of the substrate, likewise macrostructural defects or holes were not observed. Similar surface characteristics were obtained for the hybrid coating samples here evaluated, as similar results before were reported [22, 23, 34]. Homogeneity characteristics of coatings are a desired part of the roles of protective layers that consists in mitigate the corrosion into a specific corrosive environment [21]. These coatings have to improve physical barrier with anticorrosive characteristics.

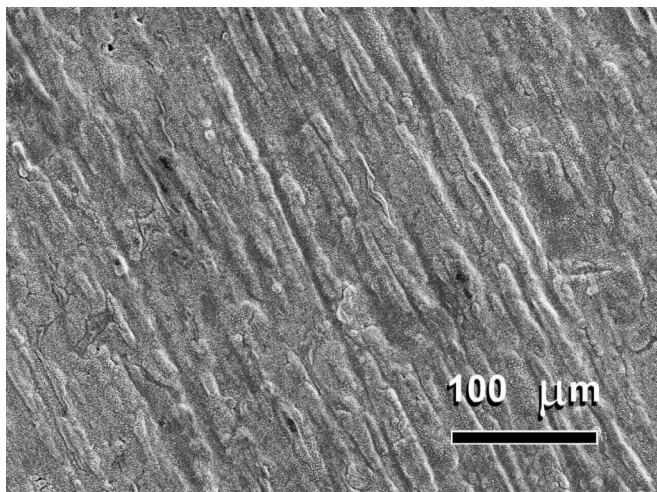


Fig. (1). SEM micrograph of the  $M_1$  coating obtained by dipcoating technique.

The role of protective films is to avoid or reduce corrosion in an acidic and basic environment [21]. The results of corrosion tests of  $M_1$  and  $C_1$  coating systems into  $\text{H}_2\text{SO}_4$  medium are shown in Figs. (2, 3). Table 1 shows the summary of the electrochemical parameters measured from these results. In the 1.0 M  $\text{H}_2\text{SO}_4$  solution, the  $M_1$  coating sample showed a decrease in corrosion current density;  $i_{corr}$ , around one order of magnitude (see Table 1). As well, its potential was reached to more positive values around of 600 mV more positive from the corrosion potential ( $E_{corr}$ ) in reference of the uncoated material. This coated sample showed an anodic behaviour with limited current density in the range of 500 mV over its  $E_{corr}$ , before the potential exceeded the breakdown potential. This behaviour was improved by the protective barrier characteristic of the coating, as before reported [23]. However,  $C_1$  coating into this solution concentration did not improve a significant change on corrosion resistance, but it showed some characteristics in the anodic current zone. In this way, the  $C_1$  coating sample presented two ranges of anodic potential of 200 mV amplitude approximately with an anodic current limit (around  $2.7 \times 10^{-3}$  and  $8.2 \times 10^{-3}$   $\text{mA/cm}^2$  respectively); before the point of the breakdown potential was reached.

One of this potential ranges was observed after the activation transition (at +140 mV of over-potential) and the second was observed at +400 mV over the  $E_{corr}$ . As a comparative result, the uncoated material presented a continuous potential range characterized by a control mechanism of equilibrium in the oxidation and reduction reactions. Also indications of breaking passive film characteristic of stainless steels were observed (curve 1 of Fig. 2). The comparison of the polarization results of behaviour of coatings material versus a self-protective substrate (SS 316) was done in order to evaluate the protective characteristics of those coatings, which could be applied in other non-self-protective structural materials to improve better corrosion resistance behaviour.

Table 1. Summary of the Electrochemical Parameters Measured from Polarization Results in the  $\text{H}_2\text{SO}_4$  Solutions

Sample	Electrolyte	$E_{corr}$ (mV)	$i_{corr}$ ( $\text{mA/cm}^2$ )	$B_a$ (mV)	$B_c$ (mV)
uncoated	1M $\text{H}_2\text{SO}_4$	+055	$3.01 \times 10^{-4}$	200	150
$M_1$		+664	$4.37 \times 10^{-5}$	195	121
$C_1$		+043	$7.14 \times 10^{-4}$	201	151
uncoated	0.1M $\text{H}_2\text{SO}_4$	-332	$6.81 \times 10^{-3}$	550	057
$M_1$		+468	$3.85 \times 10^{-5}$	140	108
$C_1$		+079	$1.73 \times 10^{-4}$	113	108

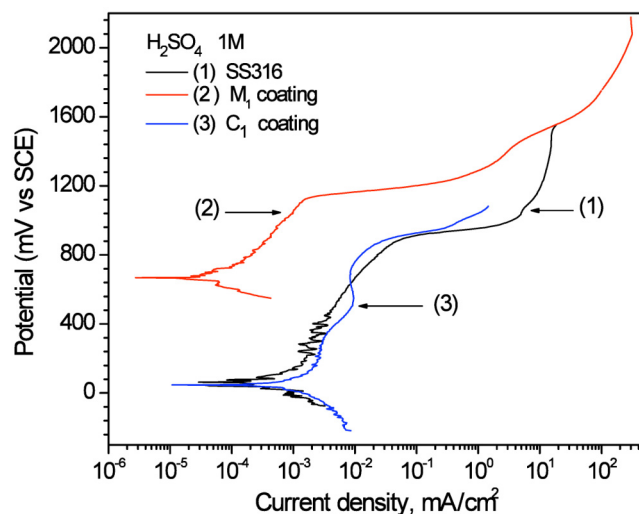


Fig. (2). Potentiodynamic polarization curves of coated SS 316 in 1M-  $\text{H}_2\text{SO}_4$  solution at 25°C.

In similar way, the polarization measurements of  $C_1$  coating sample into 0.1 M  $\text{H}_2\text{SO}_4$  solution showed better corrosion resistance behaviour than showed into the 1.0 M solution concentrations. It was reflected in a decrease of  $i_{corr}$  from 0.714 to 0.173  $\mu\text{A/cm}^2$  values; and  $E_{corr}$  potentials were without significant changes. Moreover, the  $M_1$  coating sample presented an improvement in the corrosion resistance in this solution showing values of  $i_{corr}$  in the same order (Table 1) than observed into the 1.0 M solution (Fig. 3). In this way, the  $C_1$  coating sample presented an anodic current behaviour limited on a value of  $1 \times 10^{-4}$   $\text{mA/cm}^2$  approximately in the potential range of around 600 mV

nearby to its  $E_{corr}$  potential. The limited anodic current behaviour, presented by the hybrid-oxide coating, was the characteristic of passive behaviour; and then post-passivation transition behaviour was occurred. This transition was observed at +700 mV anodic potential vs its  $E_{corr}$  (arrow *a*; Fig. 3). In this solution the  $M_1$  coating sample showed activation mechanism behaviour principally, with anodic current density controlled by oxidation and reduction reactions equilibrium. The transition of this behaviour to faster anodic dissolution (controlled by the rate of oxidation reactions) due the increase of over-potential is pointed with the arrow *b*; Fig. (3), and reached around +953 mV potential values (vs  $E_{corr}$ ) showing anodic current density values of 0.01 mA/cm<sup>2</sup> approximately. Last current density was similar to be shown by the uncoated alloy, in the anodic curve. At over-potential conditions which  $M_1$  coating showed its breakdown transition point, coating layer became to scratch faster and then exposed areas increase; as a result, corrosion current increased. We suggest that point *b* describes a start of limited current behaviour as response of the contribution capacitance of the metallic interface as an addition of a mechanism of element diffusion of alloy. In addition, the  $M_1$  coating sample showed a displacement in the  $E_{corr}$  potential to more positive values showing better corrosion resistance or lower activity, nevertheless the hybrid coating showed the best passive behaviour in a wide potential region.

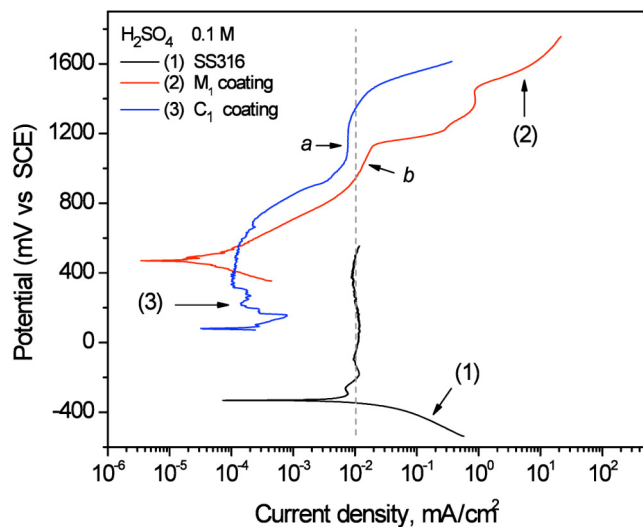


Fig. (3). Potentiodynamic polarization curves of coated SS 316 in 0.1M H<sub>2</sub>SO<sub>4</sub> solution at 25°C.

The results obtained by the potentiodynamic tests of  $M_1$  and  $C_1$  coatings in HCl solutions are showed in Figs. (4, 5). Table 2 shows the summary of the electrochemical parameters measured from these results. In this solution at 1.0 M, the uncoated stainless steel showed a more negative cell potential and bigger  $i_{corr}$ , meaning higher corrosion rate by the Tafel fitting parameters. All the coatings presented improved corrosion resistance at the OCP region. In addition, the more positive  $E_{corr}$  potential was obtained by  $M_1$  coating in 0.1 M HCl solution, while the  $E_{corr}$  of electrolyte/coating interface became more negative as the

concentration increase. On the other hand, the  $C_1$  coating had less corrosion current density ( $i_{corr}$ ) than the SS 316 substrate, just a smaller positive displacement of anodic curve, and presented the characteristic of “S” shape curve of stainless steel in this medium [35]. The most important feature of the polarization results was the electrochemical behaviour of coatings systems near the  $E_{corr}$  potential, where the coatings showed good response on corrosion resistance in HCl environment. Also the  $i_{corr}$  values were smaller than the measured ones from the uncoated material (cf. Table 2). These coatings were produced with a Si:Al = 2:1 ratio, besides coating systems with a Si:Al = 1:1 ratio previously reported [22], showed a good response with a passivation behaviour by the  $M_1$  coating system.

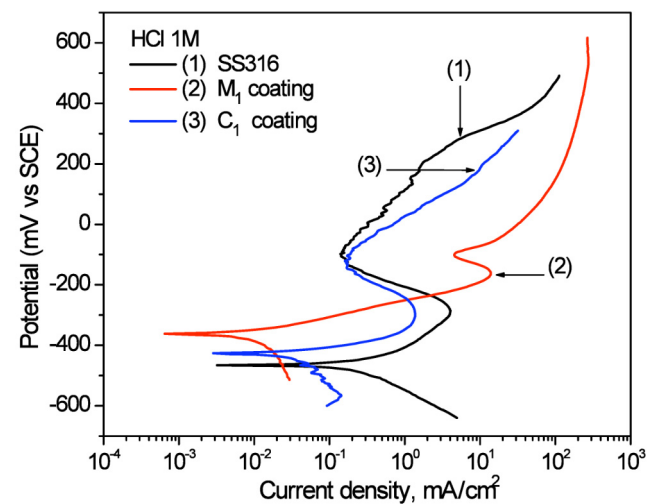


Fig. (4). Potentiodynamic polarization curves obtained in 1.0 M HCl solution at room temperature for SS 316 and coating systems.

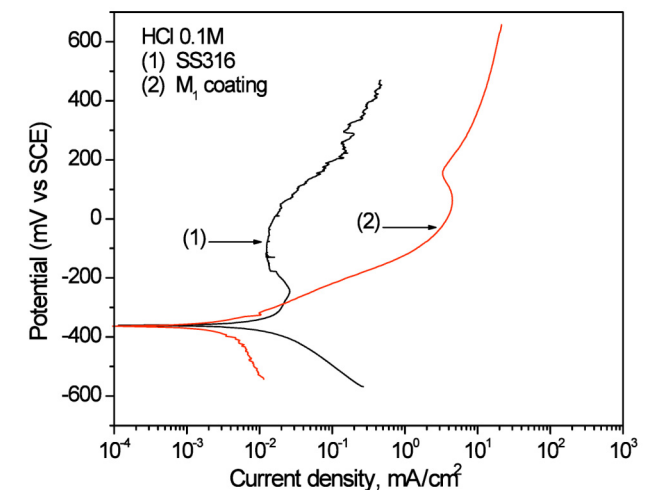


Fig. (5). Potentiodynamic polarization curves obtained in 0.1 M HCl solution at room temperature for stainless steel 316 and coating systems.

Derived from the over-potential applied, anodic current density increases with some controlled rate up to this rate increases also; this may indicate preferential localized attack, principally occurred after the electric potential exceeded the breakdown potential. This localized attack, where electrochemical reaction at the interface happens freely,

**Table 2. Summary of the Electrochemical Parameters Measured from Polarization Results in the HCl Solutions**

Sample	Electrolyte	$E_{corr}$ (mV)	$i_{corr}$ (mA/cm <sup>2</sup> )	$B_a$ (mV)	$B_c$ (mV)
uncoated	1M HCl	-465	$2.77 \times 10^{-1}$	111	126
M <sub>1</sub>		-361	$1.03 \times 10^{-2}$	053	255
C <sub>1</sub>		-427	$3.12 \times 10^{-2}$	039	235
uncoated	0.1M HCl	-358	$1.51 \times 10^{-2}$	422	167
M <sub>1</sub>		-364	$3.50 \times 10^{-3}$	99	343

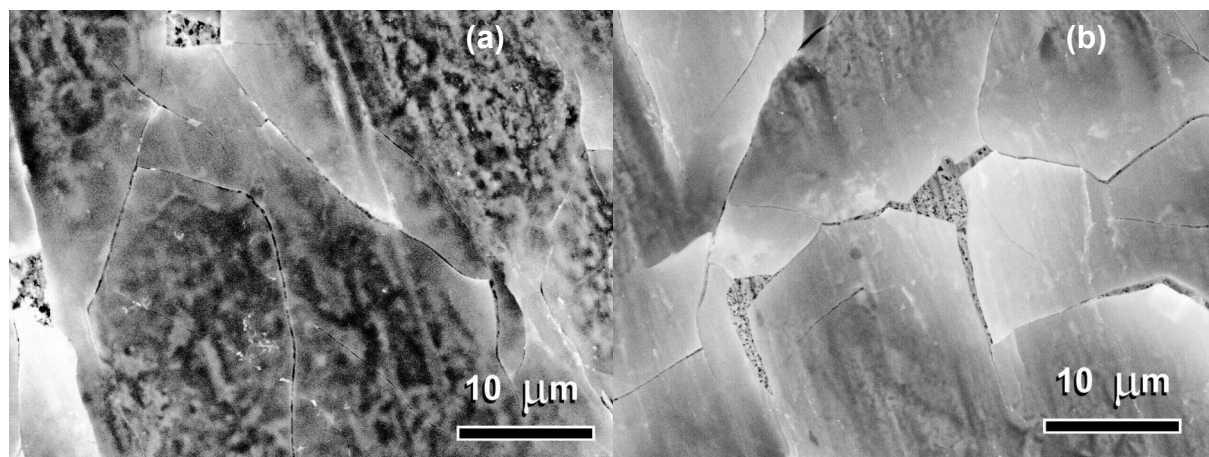
resulted in debonding, delaminating and lifting of the coating from the substrate, possibly due to hydrolysis reactions at the interface [36]. Additionally, the diffusion of the oxidant ions speeds up and the corrosion rate increases causing an accumulation of the corrosion products at the interface, promoting the formation of bulges and even leading to microcracks as it can be seen as an example in Fig. (6), before reported by Dianran *et al.* [37] also. As the corrosion products increase, the protective coating is lost by peeling of the film, such an example was the cause of the observed coating damage. Fractures of the ceramic coatings derived by the increasing of sweep over-potential initially grow from small cracking points or pitting in the coating. However, increasing higher potential promoted the cracking and peeling of the coating as shown in Fig. (6). More evident damage was observed in the M<sub>1</sub> coating in 0.1M solution (Fig. 6b), where the corrosion mechanism was mainly controlled by activation (Fig. 3). However, the coating samples showed higher corrosion resistance described by the  $E_{corr}$  and  $i_{corr}$  values (Tables 1 and 2), as reported before [22, 23, 36].

At the beginning of an interaction in a corrosive environment, the ceramic coating keeps a barrier between the substrate and environment protecting it from corrosion. Micropores and microcracks that could be present in the ceramic film play an important role in the corrosion, which generate a particular stage, high or low weight losses. In Fig. (7) we propose a different corrosion mechanism at the

interface between the sol-gel coating and the stainless steel substrate. The Schematic illustrate the possible corrosion mechanisms of coating/SS 316 interface into: a) H<sub>2</sub>SO<sub>4</sub> and b) HCl solutions. The possible paths for the electrochemical reaction between the corrosive and metal ions at the coating/substrate interface affects in the formation of an oxide layer, which could grow passive layer to enhance the corrosion resistance. Cracking during drying is a rare condition but could occur when the gel has had insufficient ageing and strength [10]. After drying, the coatings were densified by heat treatment. During this step the residual stress grows until the point of generating some microcracks into the coating. Residual stress in the interface comes from the differential thermal expansion of both substrate and film coating. However, as soon as the corrosive medium penetrates through the layer and reaches the substrate, an electrochemical reaction takes place, causing an increase of current density. Fortunately, the evaluated coatings did not show such behaviour and the surface appearance obtained by SEM characterization did not present substantial density of those defects (Fig. 1). Similar behaviour has been attributed to the presence of the methyl groups of the hybrid coatings which generate a hydrophobic barrier that restricts the access of the aqueous electrolyte into the coating pores, improving the corrosion resistance of the coating material [24].

In this sense, the affinity of sulphuric acid for water is sufficiently strong that it will remove hydrogen and oxygen atoms from other compounds. In this way, when a material reaches an over-potential condition by the dynamic polarization (as in the present work), it promotes that corrosion to take place on the metallic surface by forced way. The diffusion through the corrosion products or coating barrier increases driven by over potential force which causes an increase in the ion concentration at the interface promoting the oxidation reaction of metal. In the H<sub>2</sub>SO<sub>4</sub> solutions, the electrochemical reactions are:  $H_2SO_4 + H_2O \rightarrow H_3O^+ + HSO_4^-$ , and then  $HSO_4^- + H_2O \rightarrow H_3O^+ + SO_4^{2-}$ .

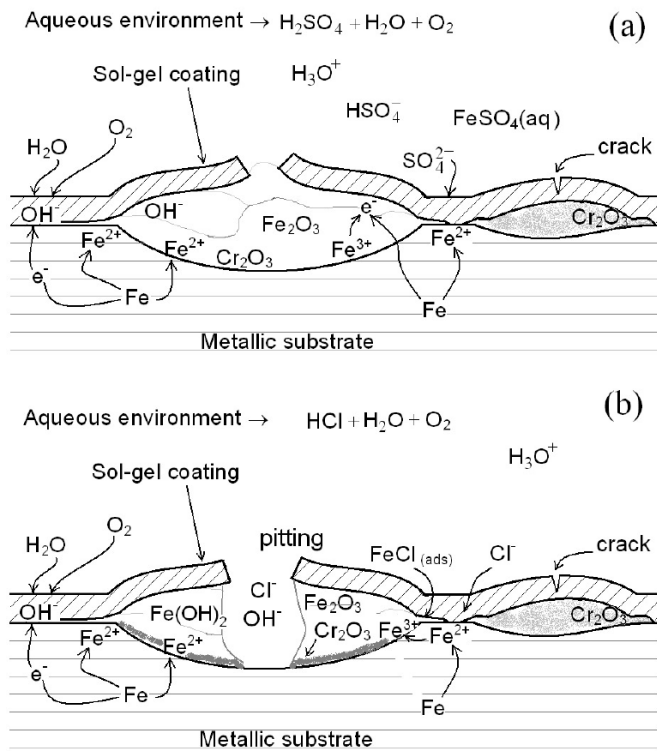
Then,  $SO_4^{2-}$  and  $O^{2-}$  ions diffusion (last from aerated solution) through metal/coating interface is driven by the over potential changes. In materials protected by ceramic coatings, this corrosion activity can promote the coating scaling by the corrosion products accumulation (schematized



**Fig. (6).** SEM micrograph of the M<sub>1</sub> coating potentiodynamic test in the H<sub>2</sub>SO<sub>4</sub> solution with: (a) 1.0 M and (b) 0.1 M concentrations. The forced damage of coating was generated by the high potential increase in the anodic region.



in Fig. 7a). As a result, formation of bulges and even leading to microcracks as it can be seen in Fig. (6), previously reported by Dianran *et al.* [37]. As the corrosion products increase, the protective coating is lost by peeling of the film, which might be the cause of the observed coating damage. Pure sulphuric acid reacts with most metals *via* a single displacement reaction to produce hydrogen gas and the metal sulphate, however, diluted  $H_2SO_4$  attacks iron, (and many metals as: aluminium, zinc, manganese, magnesium and nickel). In this way, the general reaction with iron is:  $Fe(s) + H_2SO_4(aqueous) \rightarrow H_2(g) + FeSO_4$ ; or electrochemical reaction:  $Fe^{2+} + SO_4^{2-} \rightarrow FeSO_4$ . Additionally the Cr contents an O, gives the oxidation and reduction of Cr  $\rightarrow Cr^{2+} + 2e^-$ ;  $Cr^{2+} \rightarrow Cr^{3+} + e^-$  and  $O_2 + 2e^- \rightarrow 2O^{2-}$ ; then  $2Cr^{3+} + 3O^{2-} \rightarrow Cr_2O_3$  reaction occurs at the metal/coating interface.



**Fig. (7).** Schematic illustrations of possible corrosion mechanisms (from SEM images in Fig. (6) of coating/SS 316 interface into: (a)  $H_2SO_4$  and (b)  $HCl$  solutions.

In the  $HCl$  solutions, the electrochemical reaction is:  $HCl + H_2O \rightarrow H_3O^+ + Cl^-$ . If these solutions are aerated, the oxidizing ions are compounded by  $Cl^-$  and  $O^{2-}$  ions, (Fig. 7b). The corrosion products are constituted by  $Cl$  and  $Fe$  in addition to the oxygen. These products grow easily and their structure is not protective, generating localized corrosion such pitting and crevice corrosion. The anodic metal dissolution reaction occurs principally by: oxidation of  $Fe \rightarrow Fe^{2+} + 2e^-$  then  $Fe^{2+} + 2Cl^- \rightarrow FeCl_2$ ; also  $Fe^{2+} \rightarrow Fe^{3+} + e^-$ ; and  $2Fe^{3+} + 3O^{2-} \rightarrow Fe_2O_3$ ; also  $2Cr^{3+} + 3O^{2-} \rightarrow Cr_2O_3$  happens. However, stainless steels in chloride solutions pitting corrosion, then, at the bottom of the pit,  $2Fe$

$\rightarrow 2Fe^{2+} + 4e^-$ , is balanced by the cathodic reaction at the adjacent surface,  $O_2 + 2H_2O + 4e^- \rightarrow 4OH^-$ . The increased concentration of  $Fe^{2+}$  within the pit results in the migration of chloride ions ( $Cl^-$ ) to maintain neutrality. The metal chloride formed,  $FeCl_2$ , is hydrolyzed by  $H_2O$ , hydroxide and free acid,  $FeCl_2 + 2H_2O \rightarrow Fe(OH)_2 + 2H^+ + 2Cl^-$ . This acid drops pH values at the bottom of the pit while the pH of the bulk remains neutral [38].

The kinds of corrosion products were attributed to the difference on corrosion reactions of the metal/coating interfaces in these solutions (Figs. 2-5). The reaction of substrate interface in  $H_2SO_4$  and  $HCl$  solutions promotes the interaction of  $Fe$  and  $Cr$  with the oxidizers as  $O$ , and  $S$ , and  $O$  and  $Cl$  respectively, then the formation of a protective film on the metallic surface principally by the chromium oxide minimizing the corrosion rate by passivation and spreading of microcracks. The increase of exposed area to corrosion phenomena due to coating spilling causes the increase in current density occurred at high over-potential, and explain the increase in anodic current over some ranges of potential. Nevertheless, the coatings evaluated in the current work developed good corrosion resistance, showing passivation region implied that the sol-gel coatings indeed provided a physical barrier for blocking the electrochemical corrosion process [34].

## CONCLUSIONS

Hybrid  $C_1$  and ceramic mix-oxide  $M_1$  sols were synthesized by a sol-gel process producing protective films with different properties and used to dip-coat "ormocers" coatings on SS 316. The protective properties in corrosion environments of both coating systems tested by the potentiodynamic technique suggest good corrosion resistance at OCP conditions. The  $M_1$  coatings prevent the corrosion resistance in the  $H_2SO_4$  solutions by a mechanism limited or controlled by pseudo-passivation, and presented a second passivation potential region in 0.1 M solution. Also the  $C_1$  coating developed beneficial passivation behaviour in this solution concentration.

In the  $HCl$  solutions, both coatings improved corrosion resistance at the OCP region. In addition, the more positive  $E_{corr}$  was obtained by  $M_1$  coating into 1 M  $HCl$  solution (around 100 mV more positive than substrate), and this  $E_{corr}$  became more negative as the solution concentration decrease at 0.1 M. However, the more important feature of the results was their electrochemical behaviour in the near  $E_{corr}$  region, in which the coatings shown good response of corrosion resistance. Furthermore, the  $i_{corr}$  values resulted to be smaller than  $i_{corr}$  from the uncoated material.

The origin of the deterioration of the coatings was clearly revealed by the presence of microcracks which acts as connecting pathways for the corrosive environments. The different corrosion resistance shown by protective coatings in the corrosive media was related by the development of specific corrosion products. In  $H_2SO_4$ , chromium oxides grown into metal-coating interface, which developed the best behaviour as characteristic passivation curves, while chlorine solutions generated chlorine compounds into interface cause

of bulge formations, lifting and spalling of protective coatings, thus same behaviour than uncoated material.

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