Effect of Grinding Environment on Galena Flotation

Alireza Javadi Nooshabadi and Kota Hanumantha Rao*

1Mineral Processing Group, Division of Sustainable Process Engineering, Department of Civil, Environmental and Natural Resources Engineering, Luleå University of Technology, SE-971 87 Luleå, Sweden
2Department of Geology and Mineral Resources Engineering, Norwegian University of Science and Technology, No. 7491 Trondheim, Norway

Abstract: The generation of H$_2$O$_2$ during the grinding of galena and its effect on the oxidation of galena particles leading to a decrease in flotation recovery has been studied. The influence of two types of grinding media in wet and dry grinding of galena on the formation of hydrogen peroxide and its flotation response was examined. Galena ground in mild steel grinding media generated more hydrogen peroxide compared to stainless steel media. Thus, lower flotation recovery of galena ground in mild steel could also be attributed due to the presence of higher amounts of H$_2$O$_2$ in the pulp liquid, besides widely reported galvanic interactions between grinding medium and mineral. The extent of galena surface oxidation because of either galvanic interactions or H$_2$O$_2$ presence or both, is not very clear. Clearly, both mechanisms operate in galena oxidation and needs further investigation to distinguish the predominant mechanism among the two or the extent of each contributing to surface oxidation.

Keywords: Galena, Wet and Dry Grinding, Stainless Steel and Mild Steel, Grinding Media, Hydrogen Peroxide, Flotation.

INTRODUCTION

Galena is the main mineral of lead and it is commonly associated with other sulphide minerals, such as pyrite (FeS$_2$), chalcopyrite (CuFeS$_2$) and sphalerite (ZnS). Guy and Trahar (1984) reported that the floatability of galena is dependent upon the grinding environment [1] and galena ground in a stainless mill had more recovery than in a steel mill. It was found that the oxidation–reduction environment during grinding is strongly linked to the presence of dissolved iron species from the grinding media [2]. Peng et al. (2003) observed the highest amount of iron species coating on galena particles when ground with mild steel [2]. The dissolved iron ions and their oxidation species played a dominant role in galena flotation. When galena is ground with iron as the grinding medium, galvanic interaction takes place due to a difference in their rest potentials [3, 4]. The steel grinding medium has a lower potential than galena [5]. The iron medium, which has a lower rest potential will act as the anode and galena with a higher rest potential, will act as the cathode. Electrochemical models have been proposed to explain galvanic interaction between minerals and grinding media [6]. Natarajan and Iwasaki (1984) used the electrochemical models and observed that galvanic interaction of a mild steel medium with minerals resulted in the formation of iron hydroxide species on the mineral surface [7]. Recently it was revealed that formation of hydrogen peroxide (H$_2$O$_2$), an oxidizing agent stronger than oxygen, takes place in pulp liquid during the wet grinding of complex sulphide ore [8]. Previous works showed that pyrite [9-15] chalcopyrite [14, 16], sphalerite [17] and galena [18-21] ground particles generated hydroxyl free radicals interacting with water and thus the formation of H$_2$O$_2$ in pulp liquid. Pyrite generated more H$_2$O$_2$ than other sulphide minerals and the order of H$_2$O$_2$ production by the minerals found to be pyrite > chalcopyrite > sphalerite > galena [22]. Javadi et al. (2013) showed that the mild steel generated more H$_2$O$_2$ than stainless steel grinding media since the dissolved ferrous ions play a key role in generating higher amounts of H$_2$O$_2$ [15]. Clearly, hydrogen peroxide oxidizes galena leading to its depression in flotation [23].

In our recent work we found that galena generates H$_2$O$_2$ in pH<4 [21]. In this study, the results on the effect of two types of grinding media (mild steel and stainless steel) on galena grinding in formation of hydrogen peroxide and its influence on surface oxidation and flotation recovery were presented and discussed.

MATERIALS AND METHODS

Pure galena sample used in this study was procured from Gregory, Bottley & Lloyd Ltd., United Kingdom. Galena
contains 73.69% Pb, 13.5% S, 1.38% Fe, 1.26% Zn, 0.2% Cu and some silica (quartz) impurity. The XRD analyses of the sample showed that the main mineral phase present was the galena (Fig. 1). The sample was initially crushed with a jaw crusher and screened to collect the −3.35 mm particle size fraction. Homogenised samples of 100 g each were then sealed in polyethylene bags. All flotation reagents that are being used at the Boliden sulphide mineral beneficiation plant were obtained from Boliden Mineral AB, Boliden, Sweden. Potassium amyl xanthate (KAX) and MIBC were used as collector and frother respectively. Dilute solutions of AR grade sodium hydroxide and HCl were used to maintain the desired pH value during flotation. Deionised water was used in both grinding and flotation experiments. Solutions of 2, 9-dimethyl-1, 10-phenanthroline (DMP), copper (II) sulphate (0.01 M) and phosphate buffer (pH 7.0) used in the analytical method for determining H₂O₂ and lead nitrate, ferrous sulphate and ferric sulphate used for investigating the effect of these metal ions on the formation of H₂O₂ were purchased from VWR, Sweden.

Wet Grinding and Flotation Tests

A 100 g of crushed galena sample of −3.35 mm size for each grinding test was combined with 400 ml of water and ground in a new laboratory stainless steel ball mill (Model 2VS, CAPCO Test Equipment, Suffolk, UK) either with stainless steel or mild steel media. The slurry samples during grinding were collected at pre-determined time intervals and they were immediately filtered (Millipore 0.22 µm) and the liquid (filtrate) was analysed for hydrogen peroxide.

After grinding for 60 min, the mill was emptied and the pulp was screened and it was sampled to different portions. In each flotation test, 15 g sample that was < 75 µm was transferred to a cell of 150 ml capacity (Clausthal flotation equipment), conditioned with pH modifier, collector and frother. The flotation time was 2 min at an air flow rate of 0.5 dm³ min⁻¹ in each test. The flotation froth was scraped every 10 s to collect the floated particles. The dosage of collector in flotation was 5 × 10⁻⁴ M KAX and the frother dosage was one drop of MIBC in all the tests, unless otherwise specified. The pH and collector conditioning of the pulp were 5 min and 2 min respectively. All flotation tests were performed at room temperature of approximately 22.5°C.

Dry Grinding

One hundred grams of galena was ground in a laboratory stainless steel ball mill with two types of grinding media (mild steel and stainless steel) for 60 min. After grinding, the mill was emptied and the galena was screened from grinding media. A 10 g of sample that was < 75 µm was mixed with 100 cm³ of water in a magnetic stirrer for 5 min. The slurry sample was then collected and analysed for hydrogen peroxide. The pH was regulated with HCl or NaOH solution.

Analysis of Hydrogen Peroxide

For the amount of hydrogen peroxide formation in pulp liquid, the liquid (filtrate) sample was immediately analysed by spectrophotometric method using copper (II) ions and
One millilitre each of DMP, copper (II) sulphate, and phosphate buffer (pH 7.0) solutions were added to a 10 mL volumetric flask and mixed. 1 ml of liquid (filtrate) sample was added to the volumetric flask, and then the flask was filled with ultrapure water. After mixing, the absorbance of the sample (at 454 nm) was measured with DU® Series 700 UV/Vis Scanning Spectrophotometer. The blank solution was prepared in the same manner but without H$_2$O$_2$.

**RESULTS**

**Formation of Hydrogen Peroxide (H$_2$O$_2$) During Wet Grinding and its Implications for Flotation**

The effect of the nature of grinding media on the formation of hydrogen peroxide during wet grinding of galena was investigated. The galena was wet-ground in a laboratory stainless steel ball mill with two kinds of grinding media at natural pH and slurry samples were collected at a pre-determined time intervals. The slurry samples were filtered (Millipore 0.22 µm), and the liquid (filtrate) was analysed for hydrogen peroxide. Fig. (2) shows the effect of grinding media on the formation of hydrogen peroxide where mild steel produced a higher concentration of H$_2$O$_2$ than stainless steel medium. Mild steel grinding medium was known to produce dissolved iron ions and thereby several hydrolysed iron species that adsorb on galena particles [2]. Dissolved Fe$^{2+}$ ions also react with dissolved molecular oxygen via Haber-Weiss reaction mechanism and forms superoxide anion (O$_2^-$) $\rightarrow$ (eq. 1), which reacts with ferrous iron to form H$_2$O$_2$ (eq. 2) [11].

$$\text{Fe}^{2+} + \text{O}_2 \rightarrow \text{Fe}^{3+} + (\text{O}_2^-)$$  \hspace{1cm} (1)

$$\text{Fe}^{2+} + (\text{O}_2^-) + 2\text{H}^+ \rightarrow \text{Fe}^{3+} + \text{H}_2\text{O}_2$$  \hspace{1cm} (2)

This was in agreement with other studies where mild steel produced a higher concentration of H$_2$O$_2$ than stainless steel medium during grinding of pyrite [16]. By realizing the formation of H$_2$O$_2$ in the pulp liquid, the effect of this strong oxidizing agent on solid surfaces and its consequences for flotation have been addressed below.

<table>
<thead>
<tr>
<th>pH</th>
<th>Stainless Steel</th>
<th>Mild Steel</th>
</tr>
</thead>
<tbody>
<tr>
<td>4</td>
<td>76</td>
<td>55</td>
</tr>
<tr>
<td>7</td>
<td>86</td>
<td>67</td>
</tr>
<tr>
<td>8</td>
<td>81</td>
<td>62</td>
</tr>
<tr>
<td>9</td>
<td>77</td>
<td>57</td>
</tr>
<tr>
<td>10</td>
<td>68</td>
<td>52</td>
</tr>
<tr>
<td>10.5</td>
<td>61</td>
<td>48</td>
</tr>
</tbody>
</table>

Fig. (2). Production of H$_2$O$_2$ in pulp liquid as a function of grinding time during wet grinding.

Table 1. Effect of pH on the flotation recovery of galena with air atmosphere during the flotation.
shows the effect of grinding media type on galena recovery. It can be seen that the galena wet-ground with mild steel media has a lower galena recovery than galena wet-ground with stainless steel media. This is in good agreement with other studies where 30 wt% chromium medium produced a much higher galena flotation recovery than the mild steel medium [25]. Since wet-ground galena with mild steel media produces higher amount of $\text{H}_2\text{O}_2$, a decrease in galena recovery could be due to surface oxidation caused by $\text{H}_2\text{O}_2$ oxidant. Ikumapayi et al. (2012) showed the presence of surface oxidized species such as sulfoxy and hydroxyl species on galena. [26]. Wang (2002) reported that the addition of $\text{H}_2\text{O}_2$, galena flotation decreases and completely depresses if the concentration of $\text{H}_2\text{O}_2$ exceeds $10^{-3}$ M [23]. He attributes this strong depressing action of $\text{H}_2\text{O}_2$ on galena to its strong oxidising action on lead xanthate in the galena surface which gives rise to the oxidation and decomposition of lead xanthate (eq. 3) [23].

$$[\text{Pb (EX)}_2]_{\text{ads}} + \text{H}_2\text{O}_2 \rightarrow \text{Pb (OH)}_2 + (\text{EX})_2$$

Formation of Hydrogen Peroxide ($\text{H}_2\text{O}_2$) after Dry Ground Solids are Placed in Water

The effect on the type of grinding media during dry grinding on the formation of hydrogen peroxide when the dry ground solids are placed in water was investigated. The galena was dry-ground in a laboratory stainless steel ball mill with two kinds of grinding media. Afterwards, the dry ground solids were mixed with water for 5 min. The liquid (filtrate) was analysed for hydrogen peroxide and the results are shown in Fig. (3). It can be seen that at all pH levels mild steel generated a higher concentration of $\text{H}_2\text{O}_2$ than stainless steel medium. These results correspond to the results of wet grinding (Fig. 2).

**DISCUSSION**

Tao (2004) used Eh-pH diagram to demonstrate that Mild steel medium corrodes under reducing and moderately oxidizing conditions (Fig. 4a,b) [27]. The oxidation of Mild steel yields $\text{Fe}^{2+}$ species at acid weak (pH < 6) and with a decreasing pH, $\text{Fe}^{2+}$ species increase in solution and these ferrous ions generate superoxide anion ($\text{O}_2^{-}$) in the presence of dissolved molecular oxygen (eq. 1), which reacts with ferrous iron to form $\text{H}_2\text{O}_2$ (eq. 2) [11].

Under neutral and mildly alkaline conditions, Mild steel medium does not corrode, because it is either immune under strongly reducing conditions or is in a passive state for more oxidizing conditions. In strong alkaline environments, Mild steel is free from corrosion except for a small region of potentials and pHs where soluble, alkaline, corrosion products form [27].

Tao (2004) also showed by Eh-pH diagram that stainless steel medium does not corrode in strongly reducing or oxidizing conditions except when the pH values are below 3 [27], in which case, the stainless steel is more stable than mild steel.

The proposed mechanisms of $\text{H}_2\text{O}_2$ generation are shown in Fig. (5) where $\text{Fe}^{2+}$ ions formed by mild steel are responsible for generating $\text{H}_2\text{O}_2$. 

---

**Fig. (3).** Formation of $\text{H}_2\text{O}_2$ in pulp liquid as a function of grinding time during wet grinding.
Fig. (4a). Eh-pH Diagram for Fe-O-H System, Assuming Fe(OH)₃ as Stable Fe³⁺ Phase and Activity of Dissolved Fe = 10⁻⁶ M. b) Eh-pH Diagram for Fe-Cr-H₂O System, Assuming Total Concentrations of 10⁻² M Fe and 5×10⁻³ M Cr [27].

Fig. (5). Production of H₂O₂ by galena in contact with a) Mild steel and b) Stainless steel by the incomplete reduction of oxygen (eqs. 1 and 2).
CONCLUSION
The formation of $\text{H}_2\text{O}_2$ in pulp liquid during galena grinding is more in mild steel grinding media than stainless steel and with increasing grinding time, the concentration of $\text{H}_2\text{O}_2$ increased. More flotation recovery of galena ground in stainless steel than mild steel medium is obviously due to a lower concentration of hydrogen peroxide, which acts as a strong depressant for galena.

CONFLICT OF INTEREST
The authors declare that there is no conflict of interest regarding the publication of this article.

ACKNOWLEDGEMENTS
Financial support from the research Centre for Advanced Mining and Metallurgy (CAMM), Luleå University of Technology, Luleå, Sweden, and Boliden Mineral AB, Boliden, Sweden, is gratefully acknowledged.

REFERENCES